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- Biodisintegratable thermoplatic resin moldings and a process for producing same.
- Diodisintegratable thermoplastic resin moldings and a process for producing same are disclosed, the biodisintegratable thermoplastic resin moldings being comprised of a thermoplastic aliphatic polyester resin as a matrix resin having dispersed therein another type of thermoplastic resin in a proportion of 40-75 weight % based on the whole resin. The biodisintegratable thermoplastic resin moldings are easily disintegratable after disposal in an environment where microorganisms exist so that the moldings can be reduced in bulkiness and give no harmful effect on the life of natural plants and animals. Thus, the present invention affords an effective means for solving various problems in the treatment of disposed plastic articles.

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BIODISINTEGRATABLE THERMOPLASTIC RESIN MOLDINGS AND A PROCESS FOR PRODUCING SAME

The present invention relates to biodisintegratable thermoplastic resin compositions and to a process for producing same.

In connection with the treatment of waste goods, a movement of prohibiting or limiting the use of plastics as packaging materials is being encouraged in recent years in Europe and America. In particular, biodisintegratable plastics wherein plastics are incorporated with starch are now put into practice in U.S.A. The disintegration of plastics in this case is attained by chemical decomposition of starch in the plastics by the action of microorganisms. In case the amount of starch incorporated into the plastics is small, however, the desired disintegration will not take place. On the other hand, if the amount of starch is large, the disintegration of the plastics will certainly take place, but the incorporated starch is granular and devoid of any plasticity so that the resultant resin products such as resinous sheets are significantly inferior in mechanical properties and secondary processability, such as thermoformability (in vacuum forming, pressure forming, matched die forming, etc) into containers or the like products, to ordinary plastics containing no starch. Further, the use of such biodisintegratable plastics is limited only for the manufacture of films or bags where a secondary processing treatment is not required as such.

Anyway, all of the known conventional biodisintegratable resins are unsatisfactory in maintaining mechanical properties inherent to the pure resin components and are hardly processed to manufacture shaped articles.

Under the above circumstances, there is a great demand for developing new type biodisintegratable plastics which enable disintegration by microorganisms and prevent deterioration in mechanical properties and thermoformability by incorporation of a substance chemically decomposable by microorganisms.

As a result of extensive research made by the present inventors to develop new type biodisintegratable thermoplastic resin which overcomes many drawbacks as seen in the prior art similar resins, it has now been found that compositions derived from a mixture of a biodisintegratable thermoplastic aliphatic polyester resin as a matrix and a second thermoplastics resin component as dispersant in a specific proportion exhibit excellent biodisintegratability without damaging the inherent excellent mechanical properties and secondary processability. The present invention has been accomplished on the basis of the above finding.

In accordance with the present invention, there is provided biodisintegratable thermoplastic resin composition which comprises a matrix of biodisintegratable aliphatic polyester resin having substantially uniformly dispersed therein a second thermoplastic resin component in a proportion of 40-75 weight % based on the weight of said aliphatic polyester resin and said second resin component.

In accordance with the present invention, there is also provided a process for producing a biodisintegratable thermoplastic resin composition which comprises extruding a melt-kneaded mixture of 25-60 weight % of a biodisintegratable aliphatic polyester resin and 75-40 weight % of a second thermoplastic resin component through a die positioned at the front end of an extruder under the condition satisfying the following expressions:

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10 > \eta_B/\eta_A \ge 1, preferably 5 > \eta_B/\eta_A \ge 1 (I) \eta_A 500 (II)
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wherein η_A stands for the viscosity in terms of poise of the aliphatic polyester resin at the extrusion temperature, and η_B stands for the viscosity in terms of poise of the second thermoplastic resin component at the extrusion temperature.

In the following description, the compositions of this invention are termed "moldings" in recognition of the fact that their main utility is in the production of molded articles, indeed can be directly formed as molded films, sheets, etc, as will hereafter be fully described.

The thermoplastic aliphatic polyester resin(referred to hereinafter simply as Resin A) used in the present invention as matrix resin is known and commercially available. Illustrative of Resin A are, for example, a polycondensate of an aliphatic polycarboxylic acid including dicarboxylic acid with an aliphatic polyhydric alcohol including a diol, a polycondensate of an aliphatic hydroxycarboxylic acid, and a ring-opened polycondensate of a lactone. These polymers are all biodegradable and are capable of being hydrolyzed by the action of lipase contained in microorganisms. Specific example of Resin A include homopolymers or copolymers derived from ethylene adipate, propiolactone, caprolactone and β -hydroxybutyric acid. Unlike starch, these aliphatic polyester resins are thermoplastic but fail to possess such physical properties as to make the resins alone utilizable for moldings such as a sheet or film.

Another type of the thermoplastic resin (referred to hereinafter simply as Resin B) includes various known resins conventionally used for the manufacture of moldings. Examples of Resin B are homopolymers

and copolymers derived from olefins, styrenes, vinyl compounds, acrylic compounds, lactams, and a combination of polycarboxylic acids and polyamines. Illustrative of the polymers derived from olefins are, for example, high density, medium density and low density polyethylene, polypropylene, polybutene, ethylene-propylene copolymer, propylene-butene copolymer, ethylene-vinyl acetate copolymer, etc. Illustrative of the polymers derived from styrenes are, for example, polymers or copolymers derived from styrene, methylstyrene and similar nucleus-substituted homologs. Illustrative of the polymers derived from vinyl compounds are, for example, polyvinyl chloride, polyvinylidene chloride and polyvinyl alcohol. Illustrative of the polymers derived from acrylic compounds are, for example, poly(methyl methacrylate), methyl methacrylate-styrene copolymer, methyl methacrylate-α-methylstyrene copolymer, etc. Illustrative of the polymers derived from lactams and a combination of polycarboxylic acids and polyamines are, for example, polycaprolactam and various kinds of polyamide (nylon). Other examples of Resin B include aromatic polyesters such as polyethylene terephthalate, polybutylene terephthalate, etc. Resin B is mixed as a dispersant resin with the matrix Resin A.

The biodisintegrable thermoplastic resin moldings of the present invention are distinguished by their special structure that Resin A constitutes a matrix and Resin B is uniformly dispersed therein so that Resin B is at all times covered with the biodisintegrable Resin A. As the biodisintegrable Resin A always exists on the superficial part of the resin moldings, the initial biodisintegration by microorganisms is remarkably good. After disintegration of the superficial part of the moldings by microorganisms, the newly exposed surface of the moldings also constitutes Resin A. Accordingly, the resin moldings as a whole show excellent biodisintegrability even if the moldings contain Resin B devoid of biodisintegrability.

The biodisintegrable thermoplastic resin moldings of this invention can be produced according to the process wherein a melt-kneaded mixture of the above Resins A and B in a specific proportion in an extruder is extruded through a die positioned at the front end of the extruder under the conditions satisfying the expressions (I) and (II) to a low pressure zone. Any type of the ordinary extruder can be used for this purpose.

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The extrusion conditions represented by the above expressions (I) and (II) can be achieved by using Resin A having a suitable molecular weight in conjunction with Resin B having a suitable molecular weight or by properly selecting a proportion of plural Resins A and a proportion of plural Resins B if a mixture of Resin A and a mixture of Resins B are used.

In the resin moldings of the present invention, the amount of Resin A used is 25-60 weight %, preferably 30-50 weight % and the amount of Resin B used is 75-40 weight %, preferably 70-50 weight %. As the disintegration of the moldings of this invention is caused by chemical decomposition of Resin A by microorganisms, the disintegration of the moldings is promoted by increasing the proportion of Resin A to the whole resin. If the amount of Resin A exceeds the above range, however, the mechanical properties of the resultant moldings will be deteriorated to be not practical. On the other hand, if the amount of Resin A is less than the above range, the moldings wherein Resin A constitutes a matrix resin will be not obtained even if the value η_B/η_A is increased. The moldings obtained in this case are inferior in biodegradation. If the viscosity of Resin A is less than 500 poise at the extrusion temperature, the proportion of moldings being extrusion will become difficult. If the value η_B/η_A is 10 or more, the difference in viscosity between Resin A and Resin B will become too great to be convenient in mixing both resins. On the other hand, if the value η_B/η_A is less than 1, the moldings wherein Resin A constitutes a matrix resin will not be obtained as mentioned above. Accordingly, the proportion of Resin A to Resin B and the viscosities of both resins at the extrusion temperature are specifically limited.

The moldings of this invention may be incorporated with other auxiliary substance or substances. For example, the moldings may be incorporated with an inorganic filler to enhance the mechanical strength of the moldings or with a compatibilizer to enhance miscibility of Resin A with Resin B. Illustrative of the inorganic filler are, for example, talc, calcium carbonate, magnesium carbonate, clay, silicic acid, carbon black and gypsum. Example of the compatibilizer include a copolymer of Resin A and Resin B and a polymer wherein functional groups have been introduced by great polymerization into Resin B. In case such compatibilizer is used, it is handled equivalently to Resin B so that its viscosity at the extrusion temperature c should also satisfy the equation:

 $10 > \eta_C/\eta_A \ge 1$. Further, the amount of such compatibilizer is calculated as a part of the Resin B. If necessary, the moldings may further be incorporated with a plasticizer and/or a colorant according to the intended use.

According to the above process using an extruder, the moldings of the present invention can be obtained in any desired shape, such as a film, sheet plate, thread, net and pellets. In case an injection moldings method wherein a metal die is mounted to the front end of an extruder is adopted for the production of the moldings, it is also possible to produce the moldings in any desired form of three

dimensionally large size such as a container or tray. These moldings may be foamy or solid (non-foamy) articles. It is usually determined according to the desired purpose whether foamy moldings are to be manufactured or solid moldings are to be manufactured. In case foamy moldings are produced, a known conventional foaming step is added to the above process for producing the moldings or at the separate stage the moldings have been produced. Among the above mentioned various moldings, those in the form of pellets can especially be foamed in a known conventional method at a later stage to form foamed particles which may then be molded in a mold to form articles in various forms such as cushining materials or containers. The moldings in the form of a film, sheet or plate can be shaped by a secondary processing into various articles such as a bag, bowl, tray, lunch box and cushining materials.

The biodisintegrable thermoplastic resin moldings of the present invention are easily disintegrated after disposal in an environment where microorganisms exist so that the moldings can significantly be reduced in their bulkness. Therefore, the present invention affords an effective means for solving problems of treating disposed plastic materials. Even if the moldings are left in natural environment after disposal without recovery, they are easily disintegrated by microorganisms and retain no toxic substance so that the moldings give no harmful effect on the life of natural plants and animals. The moldings of this invention are usually used in the form of a sheet, film, thread, plate, container or the like.

In particular, the moldings in the form of a film can be used for forming a cushining material having a multiplicity of air-tight cells between embossed laminated films. Such cushining material can easily be attacked after disposal by microorganisms whereby the independent hollow cells are opened to form a communicating intercellular structure. Accordingly, the moldings can be reduced in its bulkness. In case such cushining material is disposed on reclaimed land, the material is rapidly reduced in its bulkness and effectively serves to make the ground firm.

The present invention will now be illustrated in more detail by way of examples and comparative examples.

Examples 1-3, Comparative Example 1-3:

A low density polyethylene (B) having a η_B of 6,000 to 12,000 poise and a polycaprolactone (A) having a η_A of 4,000 poise at an extrusion temperature of 165 °C were melt-kneaded in a proportion as shown in Table 1 and the melt-kneaded mixture was extruded from an inflation film-producing machine having a die of 100 mm in diameter whereby a film having a thickness of about 100 μ m was obtained. The resultant film was examined for its biodisintegrability and tensile strength. The measurement of biodisintegrability in this case was conducted according to the following method: In a 100 ml Erlenmayer flask were placed 0.3 ml of a lipase solution having a factor capable of producing 130 μ mol of fatty acids in one minute from olive oil, 2 ml of a phosphate cushining solution (pH 7), 1 ml of a surfactant (trade name "Plysurf A210G", Daiichi Kogyo Seiyaku KK, Japan), 16.7 ml of water and a sample [the amount of polycaprolactone (A) is always 100 mg in each sample having a different proportion]. The mixture was then reacted together for 16 hours at 30 °C and the total organic matter formed after completion of the reaction was measured as total organic carbon(monomer and/or oligomer constituting polycaprolactone). As a control test, the experiment was carried out in the same manner as described above except that the lipase solution was not used, and the measured values were corrected on the control test.

. The measurement of tensile strength was conducted in such manner that pieces in the form of a strip of 100 mm x 10 mm were prepared and examined by means of a tensile strength tester at a distance between chucks of 50 mm and at an elongation velocity of 50 mm/min. The measurement of the viscosities (η_A and η_B) as described above was carried out by using a Shimazu's Flow Tester Model CFT-500 A (Shimazu Mfg. Co., Japan).

A result of the tests is shown in Table 1. As it is evident from Table 1, the thermoplastic resin moldings of the present invention exhibit excellent biodisintegrability and tensile strength. In contrast to this, the moldings wherein the amount of Resin A is too small (Comparative Example 2) are excellent in tensile strength but are inferior in biodisintegrability. In case of the moldings wherein the amount of Resin A is too excessive (Comparative Example 3) are excellent in biodisintegrability but are inferior in tensile strength, thus lacking in practical value.

Comparative Example 4-6:

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In case of obtaining moldings under extruding conditions satisfying the formula: $\eta_B/\eta_A > 10$ by using the resins in the same proportion as in Example 3 except that polyethylene having a viscosity (η_B) of 44,000 at 165 °C (Comparative Example 4) was used as Resin B, the difference in viscosity between the resins was

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so large that it was impossible to make the processing of the films to a film. In case of the viscosity being $\eta_B/\eta_A < 1$ in the same situation as in Example 3 except that polyethylene having a viscosity (η_B) at 165 °C of 3200 was used (Comparative Example 5), the resultant moldings in the form of a film was satisfactory in tensile strength but was deteriorated in biodisintegrability. In case of elevating the extrusion temperature to make the viscosity to $\eta_A < 500$ in the same situation as in Example 3 except that polyethylene having a viscosity (η_B) at 165 °C of 14000 was used and that polycaprolactone having a viscosity (η_A of 3000 was used (Comparative Example 6), the viscosity of the resins was too low to make processing of the resins to a film.

Examples 4-5, Comparative Examples 7-8:

A film was produced in the same manner as described in Examples 1-3 except that a polystyrene having a viscosity (η_B) of 3,000 poise or 14,000 poise was used. The resultant film was also examined for its biodisintegrability and tensile strength. A result of the examinations is shown in Table 1. As is evident from the result, the moldings of the present invention exhibit excellent biodisintegrability and tensile strength. Contrary to this, the case of the proportion of Resin A being too small (Comparative Example 7) shows good tensile strength but poor biodisintegrability. In case of using an extrusion condition of $\eta_B/\eta_A > 10$ for obtaining resin moldings (Comparative Example 8), the melt-kneaded resins were not proposed to a film.

5		Tensile	Strength	(kgf/mm^2)		1.20	1.30	1.35	3.5	4.7		1.40	0.95	-	1.35		5.0	
10	s of Film	Biodisintegrability	Against	Resin A	alone (%)	95	64	24	36	12	100	3.4	86		0.9		2.6	
15	Properties of Film	Biodisint	Organic	Substance	(mdd)	550	370	140	210	70	580	20	570		35	-	15	
20		Thickness	(und)			100	100	100	100	100	100	100	100	-	700		100	
Table 1						_												
	udition	1919				1.5	2	<u>π</u>		4.7		7	<u>.</u>	11	0.8	9	4.7	2.0
35	Extrusion Condition	N _B	-		-	0009	8000	12000	3000	14000		8000	0009	44000	3200	3600	14000	14000
40	Ext	7/a	(poise)			4000	4000	4000	3000	3000	4000	4000	4000	4000	4000	400	3000	700
45	Proportion	В	(wt8)(wt8)	·•·		45	55	65	50	65	0	85	35	65	65	65	85	99
50	Propo	4	(wt%)			55	45	35	5.0	35	100	15	65	35	35	35	15	35
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Examples 6 and 7, Comparative Example 9:

Two films of about 50 um in thickness were obtained by melt-kneading the resins in the same proportion as described in Examples 1 and 2 and in Comparative Example 2 (as shown in Table 2 below) and extruding the kneaded resins through two T dies (width: 700 mm), respectively. The resultant films were then subjected to embossing and laminating treatment by the aid of an apparatus for manufacturing bubble films Model ABM-600 (Hagino Kiko KK, Japan) whereby laminated cushining materials were obtained which had about 8550 air-tight cells about 4 mm in height and 10 mm in diameter per square meter. The resultant laminated cushining material was then examined for biodisintegrability in the following manner: First of all, 20 sheet samples (100 x 100 mm, the number of effective air-tight cells: 72) were prepared from the same laminated cushining material and piled up in a container 100 mm in length, 100 mm in width and 150 mm in height. A 2 kg weight in the form of a plate (95 mm in length and 95 mm in width) was put on the pile of the samples and the height T(A) of the 20 sheet samples was measured and recorded.

Separately, 3 ml of a lipase solution having a factor capable of producing 130 μ mol of fatty acids in one minute from olive oil, 20 ml of a phosphate cushining solution (ph 7), 10 ml of a surfactant (Plysurf A210G as described above) and 167 ml of water were placed in each of the twenty 500 ml beakers. Each sample was placed in each beaker, and the mixture in the beaker was reacted together for 48 hours at 30 °C. After completion of the reaction, each sample was taken out form the beaker and dried. The 20 sheet samples thus treated were piled up in the container and the 2 kg weight was put on the pile of the samples in the same manner as above to measure the height T(B) of the samples. From a result of the measurement, the biodisintegrability (R) of the samples was calculated according to the following equation:

 $R = [T(A) - T(B)] / T(A) \times 100 (%)$

A result of the calculation is shown in Table 2.

As is evident from the result of Table 2, the cushining material of the present invention exhibits excellent biodisintegrability as the air-tight sells are collapsed by disintegration to decrease the height, i.e. bulkness of the material rapidly. Contrary to this, the samples of Comparative Example 9 wherein the proportion of Resin A is too small did not cause collapse of the air-tight cells so that the height was not decreased.

Table 2

3	4	
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Proportion			Viscosity	y of Extrusi °C)	Biodisintegrability	
	A (wt%)	B (wt%)	η _A (poise)	η _в (poise)	ηΒ/ηΑ	R (%)
6*	55	45	4000	6000	1.5	72
7*	45	55	4000	8000	2	65
9**	15	85	4000	8000	2	3

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....Examples

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"...Comparative Example

It is understood that the preceding representative examples may be varied within the scope of the present specification both as to ingredients and treatment conditions, by one skilled in the art to achieve essentially the same results.

As many widely, different embodiments of this invention may be made without departing from the spirit and scope thereof, it is to be construed that this invention is not limited to the specific embodiment thereof except as defined in the appended claims.

Claims

1. Biodisintegratable thermoplastic resin composition which comprises a matrix of biodisintegratable aliphatic polyester resin having substantially uniformly dispersed therein a second thermoplastic resin

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component in a proportion of 40-75 weight % based on the weight of said aliphatic polyester resin and said second resin component.

- 2. Biodisintegratable thermoplastic resin composition according to Claim 1, wherein said aliphatic polyester resin is selected from a polycondensate of an aliphatic polycarboxylic acid with an aliphatic polyhydric alcohol, a polycondensate of an aliphatic hydroxycarboxylic acid, and a ring-opened polycondensate of a lactone.
- 3. Biodisintegratable thermoplastic resin composition according to Claim 1 or Claim 2, wherein said second thermoplastic resin component is selected from homopolymers or copolymers derived from olefins, styrenes, vinyl compounds, acrylic compounds, lactams, and a combination of polycarboxylic acids and polyamines.
- 4. Biodisintegratable thermoplastic resin composition according to any preceding claim, wherein said second thermoplastic resin component itself lacks biodisintegratable properties.
- 5. Biodisintegratable thermoplastic resin composition according to any preceding claim, comprising from 30-50 weight percent of said aliphatic polyester resin and correspondingly from 70-50 weight percent of said thermoplastic resin component.
- 6. Biodisintegratable thermoplastic resin composition according to any preceding claim, in the form of a molding.
- 7. Biodisintegratable thermoplastic resin composition according to Claim 6 in the form of a film, sheet or pellets.
- 8. A molded article formed from a biodisintegratable thermoplastic resin composition according to any preceding claim.
 - 9. A process for producing a biodisintegratable thermoplastic resin composition which comprises extruding a melt-kneaded mixture of 25-60 weight % of a biodisintegratable aliphatic polyester resin and 75-40 weight % of a second thermoplastic resin component through a die positioned at the front end of an extruder under the condition satisfying the following expressions:

10 >
$$\eta_{\rm B}/\eta_{\rm A} \ge 1$$
, preferably 5 > $\eta_{\rm B}/\eta_{\rm A} \ge 1$ (I) $\eta_{\rm A}$ 500 (II)

wherein η_A stands for the viscosity in terms of poise of the aliphatic polyester resin at the extrusion temperature, and η_B stands for the viscosity in terms of poise of the second thermoplastic resin component at the extrusion temperature.

- 10. A process according to Claim 9, wherein the aliphatic polyester resin is selected from a polycondensate of an aliphatic polycondensate of an aliphatic polycondensate of an aliphatic hydroxycarboxylic acid, and a ring-opened polycondensate of a lactone.
- 11. A process according to Claim 9 or Claim 10, wherein said second thermoplastic resin component is selected from homopolymers or copolymers derived from olefins, styrenes, vinyl compounds, acrylic compounds, lactams and a combination of polycarboxylic acids and polyamines.

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ם	OCUMENTS CONSI	-		
Category		h indication, where appropriate, vant passages	Relevan to claim	
×	US-A-3 929 937 (CLENDIN The whole document	INING et al.)	1-11	C 08 L 67/04 C 08 L 101/00
A	US-A-3 632 687 (E.R. WAL	TER et al.)		
A	EP-A-0 226 439 (W.R. GR.	ACE & CO.)		
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Y: A: O: P:	CATEGORY OF CITED DOCL particularly relevant if taken alone particularly relevant if combined wit document of the same catagory technological background non-written disclosure intermediate document theory or principle underlying the in	th another	the filing date D: document cited L: document cited	